

CPC COOPERATIVE PATENT CLASSIFICATION

F25J LIQUEFACTION, SOLIDIFICATION OR SEPARATION OF GASES OR GASEOUS {OR LIQUEFIED GASEOUS} MIXTURES BY PRESSURE AND COLD TREATMENT {OR BY BRINGING THEM INTO THE SUPERCRITICAL STATE (cryogenic pumps F04B 37/08; gas storage vessels, gas holders F17; filling vessels with, or discharging from vessels, compressed, liquefied or solidified gases F17C; refrigeration machines, plants, or systems F25B)}

1/00	Processes or apparatus for liquefying or solidifying gases or gaseous mixtures {(for ammonia in general C01C 1/00; solidification of carbonic acid C01B 31/22; recovering volatile solvents by condensation B01D 5/00; vapor recovery systems combined with filling nozzles B67D 7/54)(not used)}	1/008	. . {Hydrocarbons (not used)}
1/0002	. {characterised by the fluid to be liquefied (not used)}	1/0082	. . . {Methane}
1/0005	. . {Light or noble gases (F25J 1/0012 takes precedence)}	1/0085	. . . {Ethane; Ethylene}
1/0007	. . . {Helium}	1/0087	. . . {Propane; Propylene}
1/001	. . . {Hydrogen}	1/009	. . . {Hydrocarbons with four or more carbon atoms}
1/0012	. . {Primary atmospheric gases, e.g. air}	1/0092	. . . {Mixtures of hydrocarbons comprising possibly also minor amounts of nitrogen}
1/0015	. . . {Nitrogen}	1/0095	. . {Oxides of carbon, e.g. CO ₂ }
1/0017	. . . {Oxygen}	1/0097	. . {Others, e.g. F-, Cl-, HF-, HClF-, HCl-hydrocarbons etc. or mixtures thereof}
1/002	. . . {Argon}	1/02	. requiring the use of refrigeration, e.g. of helium or hydrogen {Details and kind of the refrigeration system used; Integration with other units or processes; Controlling aspects of the process (not used)}
1/0022	. . {Hydrocarbons, e.g. natural gas}	1/0201	. . {using only internal refrigeration means, i.e. without external refrigeration}
1/0025	. . . {Boil-off gases "BOG" from storages}	1/0202	. . . {in a quasi-closed internal refrigeration loop (F25J 1/0208, F25J 1/0219, F25J 1/0224 take precedence)}
1/0027	. . {Oxides of carbon, e.g. CO ₂ }	1/0203	. . {using a single-component refrigerant [SCR] fluid in a closed vapor compression cycle (F25J 1/0211 takes precedence) (not used)}
1/003	. {characterised by the kind of cold generation within the liquefaction unit for compensating heat leaks and liquid production (not used)}	1/0204	. . . {as a single flow SCR cycle}
1/0032	. . {using the feed stream itself or separated fractions from it, i.e. "internal refrigeration" (not used)}	1/0205	. . . {as a dual level SCR refrigeration cascade}
1/0035	. . . {by gas expansion with extraction of work}	1/0207	. . . {as at least a three level SCR refrigeration cascade}
1/0037 {of a return stream}	1/0208	. . . {in combination with an internal quasi-closed refrigeration loop, e.g. with deep flash recycle loop (F25J 1/021 takes precedence)}
1/004	. . . {by flash gas recovery (F25J 1/0267 takes precedence)}	1/0209 {as at least a three level refrigeration cascade}
1/0042	. . . {by liquid expansion with extraction of work}	1/021 {using a deep flash recycle loop}
1/0045	. . . {by vaporising a liquid return stream}	1/0211	. . {using a multi-component refrigerant [MCR] fluid in a closed vapor compression cycle (not used)}
1/0047	. . {using an "external" refrigerant stream in a closed vapor compression cycle (F25J 1/0221, F25J 1/0225 take precedence)(not used)}	1/0212	. . . {as a single flow MCR cycle}
1/005	. . . {by expansion of a gaseous refrigerant stream with extraction of work}	1/0214	. . . {as a dual level refrigeration cascade with at least one MCR cycle}
1/0052	. . . {by vaporising a liquid refrigerant stream}	1/0215 {with one SCR cycle}
1/0055 {originating from an incorporated cascade}	1/0216 {using a C3 pre-cooling cycle}
1/0057 {after expansion of the liquid refrigerant stream with extraction of work}	1/0217	. . . {as at least a three level refrigeration cascade with at least one MCR cycle}
1/006	. {characterised by the refrigerant fluid used (refrigerants in vapor compression cycles F25B 9/002, refrigerant materials per se C09K 5/00)(not used)}	1/0218 {with one or more SCR cycles, e.g. with a C3 pre-cooling cycle}
1/0062	. . {Light or noble gases, mixtures thereof (F25J 1/007 takes precedence)}	1/0219	. . . {in combination with an internal quasi-closed refrigeration loop, e.g. using a deep flash recycle loop}
1/0065	. . . {Helium}	1/0221	. . {using the cold stored in an external cryogenic component in an open refrigeration loop}
1/0067	. . . {Hydrogen}		
1/007	. . {Primary atmospheric gases, mixtures thereof}		
1/0072	. . . {Nitrogen}		
1/0075	. . . {Oxygen}		
1/0077	. . . {Argon}		

- 1/0222 . . . {in combination with an intermediate heat exchange fluid between the cryogenic component and the fluid to be liquefied ([F25J 1/0224 takes precedence](#))}
- 1/0223 . . . {in combination with the subsequent re-vaporisation of the originally liquefied gas at a second location to produce the external cryogenic component}
- 1/0224 . . . {in combination with an internal quasi-closed refrigeration loop ([F25J 1/0208](#), [F25J 1/0219 take precedence](#))}
- 1/0225 . . {using other external refrigeration means not provided before, e.g. heat driven absorption chillers}
- 1/0227 . . . {within a refrigeration cascade}
- 1/0228 . . {Coupling of the liquefaction unit to other units or processes, so-called integrated processes (combined plants, e.g. engine plant combined with an industrial process [F01K 23/064](#); gas turbine plants in combination with other processes [F02C 6/00](#))}
- 1/0229 . . . {Integration with a unit for using hydrocarbons, e.g. consuming hydrocarbons as feed stock}
- 1/023 {for the combustion as fuels, i.e. integration with the fuel gas system}
- 1/0231 {for the working-up of the hydrocarbon feed, e.g. reinjection of heavier hydrocarbons into the liquefied gas}
- 1/0232 . . . {integration within a pressure letdown station of a high pressure pipeline system}
- 1/0234 . . . {Integration with a cryogenic air separation unit (cryogenic separation of air [F25J 3/04](#))}
- 1/0235 . . . {Heat exchange integration}
- 1/0236 {providing refrigeration for different processes treating not the same feed stream}
- 1/0237 {integrating refrigeration provided for liquefaction and purification/treatment of the gas to be liquefied, e.g. heavy hydrocarbon removal from natural gas (details related to rectification [F25J 3/02](#); details related to partial condensation [F25J 3/06](#); working-up natural gas [C10L 3/10](#))}
- 1/0238 {Purification or treatment step is integrated within one refrigeration cycle only, i.e. the same or single refrigeration cycle provides feed gas cooling (if present) and overhead gas cooling}
- 1/0239 {Purification or treatment step being integrated between two refrigeration cycles of a refrigeration cascade, i.e. first cycle providing feed gas cooling and second cycle providing overhead gas cooling}
- 1/0241 {wherein the overhead cooling comprises providing reflux for a fractionation step}
- 1/0242 {Waste heat recovery, e.g. from heat of compression}
- 1/0243 . . {Start-up or control of the process; Details of the apparatus used; Details of the refrigerant compression system used ([not used](#))}
- 1/0244 . . . {Operation; Control and regulation; Instrumentation ([F25J 1/0279 takes precedence](#))}
- 1/0245 {Different modes, i.e. 'runs', of operation; Process control}
- 1/0247 {start-up of the process}
- 1/0248 {Stopping of the process, e.g. defrosting or deriming, maintenance; Back-up mode or systems}
- 1/0249 {Controlling refrigerant inventory, i.e. composition or quantity ([charging or discharging refrigerants in cooling systems F25B 45/00](#))}
- 1/025 {Details related to the refrigerant production or treatment, e.g. make-up supply from feed gas itself}
- 1/0251 {Intermittent or alternating process, so-called batch process, e.g. "peak-shaving"}
- 1/0252 {Control strategy, e.g. advanced process control or dynamic modeling}
- 1/0254 {controlling particular process parameter, e.g. pressure, temperature}
- 1/0255 {controlling the composition of the feed or liquefied gas, e.g. to achieve a particular heating value of natural gas}
- 1/0256 {Safety aspects of operation ([F25J 1/0298 takes precedence](#))}
- 1/0257 . . . {Construction and layout of liquefaction equipments, e.g. valves, machines ([F25J 1/0279 takes precedence](#))}
- 1/0258 {vertical layout of the equipments within in the cold box}
- 1/0259 {Modularity and arrangement of parts of the liquefaction unit and in particular of the cold box, e.g. pre-fabrication, assembling and erection, dimensions, horizontal layout "plot"}
- 1/0261 {Details of cold box insulation, housing and internal structure ([buildings forming parts of cooling plants E04H 5/10](#))}
- 1/0262 {Details of the cold heat exchange system (constructional details [F25J 5/00](#), construction of cold-exchangers in general [F28](#))}
- 1/0263 {using different types of heat exchangers}
- 1/0264 {Arrangement of heat exchanger cores in parallel with different functions, e.g. different cooling streams ([F25J 1/0272 takes precedence](#))}
- 1/0265 {comprising cores associated exclusively with the cooling of a refrigerant stream, e.g. for auto-refrigeration or economizer}
- 1/0267 {using flash gas as heat sink}
- 1/0268 {using a dedicated refrigeration means ([F25J 1/0296 takes precedence](#))}
- 1/0269 {Arrangement of liquefaction units or equipments fulfilling the same process step, e.g. multiple "trains" concept ([F25J 1/0294 takes precedence](#))}
- 1/027 {Inter-connecting multiple hot equipments upstream of the cold box}
- 1/0271 {Inter-connecting multiple cold equipments within or downstream of the cold box}
- 1/0272 {Multiple identical heat exchangers in parallel}

1/0274 {Retrofitting or revamping of an existing liquefaction unit}	3/0219 {Refinery gas, cracking gas, coke oven gas, gaseous mixtures containing aliphatic unsaturated CnHm or gaseous mixtures of undefined nature}
1/0275 {adapted for special use of the liquefaction unit, e.g. portable or transportable devices}	3/0223 {H ₂ /CO mixtures, i.e. synthesis gas; Water gas or shifted synthesis gas (production of carbon monoxide containing gas in general C01B 31/18 , C10J , C10K ; production of hydrogen containing gas C01B 3/00)}
1/0276 {Laboratory or other miniature devices}	3/0228	. . {characterised by the separated product stream (not used)}
1/0277 {Offshore use, e.g. during shipping}	3/0233 {separation of CnHm with 1 carbon atom or more}
1/0278 {Unit being stationary, e.g. on floating barge or fixed platform}	3/0238 {separation of CnHm with 2 carbon atoms or more}
1/0279 {Compression of refrigerant or internal recycle fluid, e.g. kind of compressor, accumulator, suction drum etc.}	3/0242 {separation of CnHm with 3 carbon atoms or more}
1/0281 {characterised by the type of prime driver, e.g. hot gas expander}	3/0247 {separation of CnHm with 4 carbon atoms or more}
1/0282 {Steam turbine as the prime mechanical driver}	3/0252 {separation of hydrogen (production of hydrogen containing gas in general C01B 3/00 , e.g. separation of hydrogen or hydrogen containing gases form gaseous mixtures at low temperatures C01B 3/506)}
1/0283 {Gas turbine as the prime mechanical driver}	3/0257 {separation of nitrogen (from air F25J 3/04 , production of nitrogen in general C01B 21/00)}
1/0284 {Electrical motor as the prime mechanical driver}	3/0261 {separation of carbon monoxide (production of carbon monoxide containing gas in general C01B 31/18 , C10J , C10K)}
1/0285 {Combination of different types of drivers mechanically coupled to the same refrigerant compressor, possibly split on multiple compressor casings}	3/0266 {separation of carbon dioxide (production of carbon dioxide in general C01B 31/00)}
1/0287 {including an electrical motor}	3/0271 {separation of H ₂ /CO mixtures, i.e. of synthesis gas (production of carbon monoxide containing gas in general C01B 31/18 , C10J , C10K , production of hydrogen containing gas C01B 3/00)}
1/0288 {using work extraction by mechanical coupling of compression and expansion of the refrigerant, so-called companders}	3/0276 {separation of H ₂ /N ₂ mixtures, i.e. of ammonia synthesis gas (in general C01B 3/00)}
1/0289 {Use of different types of prime drivers of at least two refrigerant compressors in a cascade refrigeration system}	3/028 {separation of noble gases (from air F25J 3/04642 ; in general C01B 23/00)}
1/029 {Mechanically coupling of different refrigerant compressors in a cascade refrigeration system to a common driver}	3/0285 {of argon}
1/0291 {Refrigerant compression by combined gas compression and liquid pumping}	3/029 {of helium}
1/0292 {Refrigerant compression by cold or cryogenic suction of the refrigerant gas}	3/0295	. . {Start-up or control of the process; Details of the apparatus used, e.g. sieve plates, packings}
1/0294 {Multiple compressor casings/strings in parallel, e.g. split arrangement}	3/04	. . for air {(not used)}
1/0295 {Shifting of the compression load between different cooling stages within a refrigerant cycle or within a cascade refrigeration system}	3/04006 {Providing pressurised feed air or process streams within or from the air fractionation unit (not used)}
1/0296 {Removal of the heat of compression, e.g. within an inter- or afterstage-cooler against an ambient heat sink}	3/04012 {by compression of warm gaseous streams; details of intake or interstage cooling (F25J 3/04048 takes precedence; operation of compressors F25J 3/04781 ; particular layout of compressors used in air fractionation units F25J 3/04866)}
1/0297 {using an externally chilled fluid, e.g. chilled water}	3/04018 {of main feed air}
1/0298 {Safety aspects and control of the refrigerant compression system, e.g. anti-surge control}	3/04024 {of purified feed air, so-called boosted air}
3/00	Processes or apparatus for separating the constituents of gaseous {or liquefied gaseous} mixtures involving the use of liquefaction or solidification {(not used)}	3/0403 {of nitrogen}
3/02	. by rectification, i.e. by continuous interchange of heat and material between a vapour stream and a liquid stream (F25J 3/08 takes precedence; {purification of hydrocarbons in general C07C 7/00 ; not used})	3/04036 {of oxygen}
3/0204	. . {characterised by the feed stream (for air F25J 3/04)(not used)}	3/04042 {of argon or argon enriched stream}
3/0209 {Natural gas or substitute natural gas}	3/04048 {by compression of cold gaseous streams, e.g. intermediate or oxygen enriched (waste) streams}
3/0214 {Liquefied natural gas}	3/04054 {of air}
		3/0406 {of nitrogen}

- 3/04066 {of oxygen}
- 3/04072 {of argon or argon enriched stream}
- 3/04078 {providing pressurized products by liquid compression and vaporisation with cold recovery, i.e. so-called internal compression (operation of pumps [F25J 3/04781](#); particular layout of pumps used in air fractionation units [F25J 3/04866](#))}
- 3/04084 {of nitrogen}
- 3/0409 {of oxygen}
- 3/04096 {of argon or argon enriched stream}
- 3/04103 {using solely hydrostatic liquid head}
- 3/04109 {Arrangements of compressors and /or their drivers (using work extraction by mechanical coupling of compression and cold expansion [F25J 3/04381](#))}
- 3/04115 {characterised by the type of prime driver, e.g. hot gas expander}
- 3/04121 {Steam turbine as the prime mechanical driver}
- 3/04127 {Gas turbine as the prime mechanical driver}
- 3/04133 {Electrical motor as the prime mechanical driver}
- 3/04139 {Combination of different types of drivers mechanically coupled to the same compressor, possibly split on multiple compressor casings}
- 3/04145 {Mechanically coupling of different compressors of the air fractionation process to the same driver(s)}
- 3/04151 {Purification and (pre-)cooling of the feed air; recuperative heat-exchange with product streams (not used)}
- 3/04157 {Afterstage cooling and so-called "pre-cooling" of the feed air upstream the air purification unit and main heat exchange line ([F25J 3/04618](#) takes precedence)}
- 3/04163 {Hot end purification of the feed air (arrangements of cold regenerators [F25J 5/00](#))}
- 3/04169 {by adsorption of the impurities (adsorption in general [B01D 53/02](#))}
- 3/04175 {at a pressure of substantially more than the highest pressure column}
- 3/04181 {Regenerating the adsorbents}
- 3/04187 {Cooling of the purified feed air by recuperative heat-exchange; Heat-exchange with product streams (arrangements of cold exchangers [F25J 5/002](#))}
- 3/04193 {Division of the main heat exchange line in consecutive sections having different functions}
- 3/042 {having an intermediate feed connection}
- 3/04206 {including a so-called "auxiliary vaporiser" for vaporising and producing a gaseous product}
- 3/04212 {and simultaneously condensing vapor from a column serving as reflux within the or another column}
- 3/04218 {Parallel arrangement of the main heat exchange line in cores having different functions, e.g. in low pressure and high pressure cores ([F25J 3/04503](#) takes precedence)}
- 3/04224 {Cores associated with a liquefaction or refrigeration cycle}
- 3/0423 {Subcooling of liquid process streams}
- 3/04236 {Integration of different exchangers in a single core, so-called integrated cores ([F25J 3/04624](#) takes precedence)}
- 3/04242 {Cold end purification of the feed air}
- 3/04248 {Generation of cold for compensating heat leaks or liquid production, e.g. by Joule-Thompson expansion}
- 3/04254 {using the cold stored in external cryogenic fluids ([closed loop F25J 3/04278](#))}
- 3/0426 {The cryogenic component does not participate in the fractionation}
- 3/04266 {and being liquefied hydrocarbons}
- 3/04272 {and comprising means for reducing the risk of pollution of hydrocarbons into the air fractionation}
- 3/04278 {using external refrigeration units, e.g. closed mechanical or regenerative refrigeration units}
- 3/04284 {using internal refrigeration by open-loop gas work expansion, e.g. of intermediate or oxygen enriched (waste-)streams ([F25J 3/04333](#) takes precedence)}
- 3/0429 {of feed air, e.g. used as waste or product air or expanded into an auxiliary column}
- 3/04296 {Claude expansion, i.e. expanded into the main or high pressure column}
- 3/04303 {Lachmann expansion, i.e. expanded into oxygen producing or low pressure column}
- 3/04309 {of nitrogen}
- 3/04315 {Lowest pressure or impure nitrogen, so-called waste nitrogen expansion}
- 3/04321 {of oxygen}
- 3/04327 {of argon or argon enriched stream}
- 3/04333 {using quasi-closed loop internal vapor compression refrigeration cycles, e.g. of intermediate or oxygen enriched (waste-)streams}
- 3/04339 {of air}
- 3/04345 {and comprising a gas work expansion loop}
- 3/04351 {of nitrogen}
- 3/04357 {and comprising a gas work expansion loop}
- 3/04363 {of oxygen}
- 3/04369 {of argon or argon enriched stream}
- 3/04375 {Details relating to the work expansion, e.g. process parameter etc.}
- 3/04381 {using work extraction by mechanical coupling of compression and expansion so-called companders}
- 3/04387 {using liquid or hydraulic turbine expansion}
- 3/04393 {using multiple or multistage gas work expansion}

- 3/044 . . . {using a single pressure main column system only ([F25J 3/0446](#), [F25J 3/04624](#), [F25J 3/04636](#) take precedence)}
- 3/04406 . . . {using a dual pressure main column system ([F25J 3/0446](#), [F25J 3/04624](#), [F25J 3/04636](#) and [F25J 3/04715](#) take precedence)(not used)}
- 3/04412 {in a classical double column flowsheet, i.e. with thermal coupling by a main reboiler-condenser in the bottom of low pressure respectively top of high pressure column}
- 3/04418 {with thermally overlapping high and low pressure columns}
- 3/04424 {without thermally coupled high and low pressure columns, i.e. a so-called split columns}
- 3/0443 {A main column system not otherwise provided, e.g. a modified double column flowsheet}
- 3/04436 . . . {using at least a triple pressure main column system ([F25J 3/0446](#), [F25J 3/04624](#), [F25J 3/04636](#) and [F25J 3/04715](#) take precedence)(not used)}
- 3/04442 {in a double column flowsheet with a high pressure pre-rectifier}
- 3/04448 {in a double column flowsheet with an intermediate pressure column}
- 3/04454 {a main column system not otherwise provided, e.g. serially coupling of columns or more than three pressure levels}
- 3/0446 . . . {using the heat generated by mixing two different phases}
- 3/04466 {for producing oxygen as a mixing column overhead gas by mixing gaseous air feed and liquid oxygen}
- 3/04472 . . . {using the cold from cryogenic liquids produced within the air fractionation unit and stored in internal or intermediate storages (not used)}
- 3/04478 {for controlling purposes, e.g. start-up or back-up procedures ([F25J 3/04496](#) takes precedence)}
- 3/04484 {for purity control during steady state operation}
- 3/0449 {for rapid load change of the air fractionation unit}
- 3/04496 {for compensating variable air feed or variable product demand by alternating between periods of liquid storage and liquid assist}
- 3/04503 {by exchanging "cold" between at least two different cryogenic liquids, e.g. independently from the main heat exchange line of the air fractionation and/or by using external alternating storage systems}
- 3/04509 {within the cold part of the air fractionation, i.e. exchanging "cold" within the fractionation and/or main heat exchange line}
- 3/04515 {Simultaneously changing air feed and products output}
- 3/04521 {Coupling of the air fractionation unit to an air gas-consuming unit, so-called integrated processes (combined plants, e.g. engine plant combined with an industrial process [F01K 23/064](#); gas-turbine plants supplying working fluid to a chemical process [F02C 6/10](#))(not used)}
- 3/04527 {Integration with an oxygen consuming unit, e.g. glass facility, waste incineration or oxygen based processes in general}
- 3/04533 {for the direct combustion of fuels in a power plant, so-called "oxyfuel combustion"}
- 3/04539 {for the H_2/CO synthesis by partial oxidation or oxygen consuming reforming processes of fuels}
- 3/04545 {for the gasification of solid or heavy liquid fuels, e.g. integrated gasification combined cycle [IGCC]}
- 3/04551 {for the metal production}
- 3/04557 {for pig iron or steel making, e.g. blast furnace, Corex}
- 3/04563 {Integration with an nitrogen consuming unit, e.g. for purging, inerting, cooling or heating}
- 3/04569 {for enhanced or tertiary oil recovery}
- 3/04575 {for a gas expansion plant, e.g. dilution of the combustion gas in a gas turbine}
- 3/04581 {Hot gas expansion of indirect heated nitrogen}
- 3/04587 {for the NH_3 synthesis, e.g. for adjusting the H_2/N_2 ratio}
- 3/04593 {The air gas consuming unit is also fed by an air stream}
- 3/046 {Completely integrated air feed compression, i.e. common MAC}
- 3/04606 {Partially integrated air feed compression, i.e. independent MAC for the air fractionation unit plus additional air feed from the air gas consuming unit}
- 3/04612 {Heat exchange integration with process streams, e.g. from the air gas consuming unit}
- 3/04618 {for cooling an air stream fed to the air fractionation unit}
- 3/04624 . . . {using integrated mass and heat exchange, so-called non-adiabatic rectification, e.g. dephlegmator, reflux exchanger}
- 3/0463 {Simultaneously between rectifying and stripping sections, i.e. double dephlegmator}
- 3/04636 . . . {using a hybrid air separation unit, e.g. combined process by cryogenic separation and non-cryogenic separation techniques ([F25J 3/04733](#) and [F25J 3/04757](#) take precedence)}
- 3/04642 . . . {Recovering noble gases from air (from gas mixtures other than air [F25J 3/028](#) or [F25J 3/0685](#))}
- 3/04648 {argon (not used)}
- 3/04654 {Producing crude argon in a crude argon column}
- 3/0466 {as a parallel working rectification column or auxiliary column system in a single pressure main column system}

- 3/04666 {as a parallel working rectification column of the low pressure column in a dual pressure main column system}
- 3/04672 {having a top condenser}
- 3/04678 {cooled by oxygen enriched liquid from high pressure column bottoms}
- 3/04684 {and a bottom re-boiler [\(F25J 3/04696 takes precedence\)](#)}
- 3/0469 {and an intermediate re-boiler/condenser [\(F25J 3/04696 takes precedence\)](#)}
- 3/04696 {a bottom re-boiler and an intermediate re-boiler/condenser}
- 3/04703 {being arranged in more than one vessel}
- 3/04709 {as an auxiliary column system in at least a dual pressure main column system}
- 3/04715 {The auxiliary column system simultaneously produces oxygen}
- 3/04721 {Producing pure argon, e.g. recovered from a crude argon column}
- 3/04727 {using an auxiliary pure argon column for nitrogen rejection [\(F25J 3/04739 takes precedence\)](#)}
- 3/04733 {using a hybrid system, e.g. using adsorption, permeation or catalytic reaction}
- 3/04739 {in combination with an auxiliary pure argon column}
- 3/04745 {Krypton and/or Xenon}
- 3/04751 {Producing pure krypton and/or xenon recovered from a crude krypton/xenon mixture}
- 3/04757 {using a hybrid system, e.g. using adsorption, permeation or catalytic reaction}
- 3/04763 {Start-up or control of the process; Details of the apparatus used [\(not used\)](#)}
- 3/04769 {Operation, control and regulation of the process; Instrumentation within the process}
- 3/04775 {Air purification and pre-cooling}
- 3/04781 {Pressure changing devices, e.g. for compression, expansion, liquid pumping}
- 3/04787 {Heat exchange, e.g. main heat exchange line; Subcooler, external reboiler-condenser [\(F25J 3/04793 and F25J 3/0486 take precedence\)](#)}
- 3/04793 {Rectification, e.g. columns; Reboiler-condenser [\(F25J 3/0486 takes precedence\)](#)}
- 3/048 {Argon recovery}
- 3/04806 {High purity argon purification}
- 3/04812 {Different modes, i.e. "runs" of operation [\(F25J 3/04472 takes precedence\)](#)}
- 3/04818 {Start-up of the process}
- 3/04824 {Stopping of the process, e.g. defrosting or deriming; Back-up procedures}
- 3/0483 {Rapid load change of the air fractionation unit}
- 3/04836 {Variable air feed, i.e. "load" or product demand during specified periods, e.g. during periods with high respectively low power costs [\(F25J 3/0483 takes precedence\)](#)}
- 3/04842 {Intermittent process, so-called batch process}
- 3/04848 {Control strategy, e.g. advanced process control or dynamic modeling}
- 3/04854 {Safety aspects of operation}
- 3/0486 {of vaporisers for oxygen enriched liquids, e.g. purging of liquids}
- 3/04866 {Construction and layout of air fractionation equipments, e.g. valves, machines [\(F25J 5/00 takes precedence\)](#)}
- 3/04872 {Vertical layout of cold equipments within in the cold box, e.g. columns, heat exchangers etc.}
- 3/04878 {Side by side arrangement of multiple vessels in a main column system, wherein the vessels are normally mounted one upon the other or forming different sections of the same column [\(multiple vessels of a crude argon column F25J 3/04703\)](#)}
- 3/04884 {Arrangement of reboiler-condensers}
- 3/0489 {Modularity and arrangement of parts of the air fractionation unit, in particular of the cold box, e.g. pre-fabrication, assembling and erection, dimensions, horizontal layout "plot" [\(F25J 3/04872 takes precedence\)](#)}
- 3/04896 {Details of columns, e.g. internals, inlet/outlet devices}
- 3/04903 {Plates or trays}
- 3/04909 {Structured packings}
- 3/04915 {Combinations of different material exchange elements, e.g. within different columns}
- 3/04921 {within the same column}
- 3/04927 {Liquid or gas distribution devices}
- 3/04933 {Partitioning walls or sheets}
- 3/04939 {Vertical, e.g. dividing wall columns [\(details of dephlegmators F25J 5/007\)](#)}
- 3/04945 {Details of internal structure; insulation and housing of the cold box}
- 3/04951 {Arrangements of multiple air fractionation units or multiple equipments fulfilling the same process step, e.g. multiple trains in a network [\(F25J 3/04636 takes precedence\)](#)}
- 3/04957 {and inter-connecting equipments upstream of the fractionation unit (s), i.e. at the "front-end"}
- 3/04963 {and inter-connecting equipment within or downstream of the fractionation unit(s) [\(F25J 3/04393 takes precedence\)](#)}
- 3/04969 {Retrofitting or revamping of an existing air fractionation unit}
- 3/04975 {adapted for special use of the air fractionation unit, e.g. transportable devices by truck or small scale use}
- 3/04981 {for portable medical or home use}

3/04987 {for offshore use}	5/007	. . {combined with mass exchange, i.e. in a so-called dephlegmator}
3/04993 {for space applications, e.g. for rocket use}		
3/06	. by partial condensation (F25J 3/08 takes precedence; by rectification F25J 3/02; {purification of hydrocarbons in general C07C 7/00; not used})	2200/00	Processes or apparatus using separation by rectification (not used)
3/0605	. . {characterised by the feed stream (for air F25J 3/04)(not used)}	2200/02	. in a single pressure main column system
3/061	. . . {Natural gas or substitute natural gas}	2200/04	. in a dual pressure main column system
3/0615 {Liquefied natural gas}	2200/06	. . in a classical double column flow-sheet, i.e. with thermal coupling by a main reboiler-condenser in the bottom of low pressure respectively top of high pressure column
3/062	. . . {Refinery gas, cracking gas, coke oven gas, gaseous mixtures containing aliphatic unsaturated CnHm or gaseous mixtures of undefined nature}	2200/08	. in a triple pressure main column system
3/0625	. . . {H ₂ /CO mixtures, i.e. synthesis gas; Water gas or shifted synthesis gas (production of carbon monoxide containing gas in general C01B 31/18, C10J, C10K; production of hydrogen containing gas C01B 3/00)}	2200/10	. in a quadruple, or more, column or pressure system
3/063	. . {characterised by the separated product stream (not used)}	2200/20	. in an elevated pressure multiple column system wherein the lowest pressure column is at a pressure well above the minimum pressure needed to overcome pressure drop to reject the products to atmosphere
3/0635	. . . {separation of CnHm with 1 carbon atom or more}	2200/30	. using a side column in a single pressure column system
3/064	. . . {separation of CnHm with 2 carbon atoms or more}	2200/32	. using a side column fed by a stream from the high pressure column
3/0645	. . . {separation of CnHm with 3 carbon atoms or more}	2200/34	. using a side column fed by a stream from the low pressure column
3/065	. . . {separation of CnHm with 4 carbon atoms or more}	2200/38	. using pre-separation or distributed distillation before a main column system, e.g. in a at least a double column system
3/0655	. . . {separation of hydrogen (production of hydrogen containing gas in general C01B 3/00, e.g. separation of hydrogen or hydrogen containing gases form gaseous mixtures at low temperatures C01B 3/506)}	2200/40	. Features relating to the provision of boil-up in the bottom of a column
3/066	. . . {separation of nitrogen (from air F25J 3/04, production of nitrogen in general C01B 21/00)}	2200/50	. using multiple (re-)boiler-condensers at different heights of the column
3/0665	. . . {separation of carbon monoxide (production of carbon monoxide containing gas in general C01B 31/18, C10J, C10K)}	2200/52	. . in the high pressure column of a double pressure main column system
3/067	. . . {separation of carbon dioxide (production of carbon dioxide in general C01B 31/00)}	2200/54	. . in the low pressure column of a double pressure main column system
3/0675	. . . {separation of H ₂ /CO mixtures, i.e. of synthesis gas (production of carbon monoxide containing gas in general C01B 31/18, C10J, C10K, production of hydrogen containing gas C01B 3/00)}	2200/70	. Refluxing the column with a condensed part of the feed stream, i.e. fractionator top is stripped or self-rectified
3/068	. . . {separation of H ₂ /N ₂ mixtures, i.e. of ammonia synthesis gas (in general C01B 31/00)}	2200/72	. Refluxing the column with at least a part of the totally condensed overhead gas
3/0685	. . . {separation of noble gases (from air F25J 3/04642; in general C01B 23/00)}	2200/74	. Refluxing the column with at least a part of the partially condensed overhead gas
3/069 {of helium}	2200/76	. Refluxing the column with condensed overhead gas being cycled in a quasi-closed loop refrigeration cycle
3/0695	. . {Start-up or control of the process; Details of the apparatus used}	2200/78	. Refluxing the column with a liquid stream originating from an upstream or downstream fractionator column
3/08	. Separating gaseous impurities from gases or gaseous mixtures {or from liquefied gases or liquefied gaseous mixtures} (cold traps B01D 8/00)	2200/80	. using integrated mass and heat exchange, i.e. non-adiabatic rectification in a reflux exchanger or dephlegmator
5/00	Arrangements of cold exchangers or cold accumulators in separation or liquefaction plants (heat exchangers F28C, F28D, F28F)	2200/90	. Details relating to column internals, e.g. structured packing, gas or liquid distribution
5/002	. {for continuously recuperating cold, i.e. in a so-called recuperative heat exchanger}	2200/92	. . Details relating to the feed point
5/005	. . {in a reboiler-condenser, e.g. within a column}	2200/94	. . Details relating to the withdrawal point
		2200/96	. . Dividing wall column
		<NO TITLE>	
		2205/00	Processes or apparatus using other separation and/or other processing means (not used)
		2205/02	. using simple phase separation in a vessel or drum
		2205/04	. . in the feed line, i.e. upstream of the fractionation step

2205/10	• using combined expansion and separation, e.g. in a vortex tube, "Ranque tube" or a "cyclonic fluid separator", i.e. combination of an isentropic nozzle and a cyclonic separator; Centrifugal separation	2210/80	• Carbon dioxide
2205/20	• using solidification of components	2210/90	• Boil-off gas from storage
2205/24	• using regenerators, cold accumulators or reversible heat exchangers	2215/00	Processes characterised by the type or other details of the product stream (not used)
2205/30	• using a washing, e.g. "scrubbing" or bubble column for purification purposes	2215/02	• Mixing or blending of fluids to yield a certain product
2205/32	• • as direct contact cooling tower to produce a cooled gas stream, e.g. direct contact after cooler [DCAC]	2215/04	• Recovery of liquid products
2205/34	• • as evaporative cooling tower to produce chilled water, e.g. evaporative water chiller [EWC]	2215/10	• Hydrogen
2205/40	• using hybrid system, i.e. combining cryogenic and non-cryogenic separation techniques	2215/14	• Carbon monoxide
2205/50	• using absorption, i.e. with selective solvents or lean oil, heavier CnHm and including generally a regeneration step for the solvent or lean oil	2215/18	• HYCO synthesis gas, e.g. H ₂ /CO mixture
2205/60	• using adsorption on solid adsorbents, e.g. by temperature-swing adsorption [TSA] at the hot or cold end	2215/20	• Ammonia synthesis gas, e.g. H ₂ /N ₂ mixture
2205/62	• • Purifying more than one feed stream in multiple adsorption vessels, e.g. for two feed streams at different pressures	2215/30	• Helium
2205/64	• • by pressure-swing adsorption [PSA] at the hot end	2215/32	• Neon
2205/66	• • Regenerating the adsorption vessel, e.g. kind of reactivation gas	2215/34	• Krypton
2205/68	• • • Cooling the adsorption vessel	2215/36	• Xenon
2205/70	• • • Heating the adsorption vessel	2215/40	• Air or oxygen enriched air, i.e. generally less than 30mol% of O ₂
2205/72	• • • Pressurising or depressurising the adsorption vessel	2215/42	• Nitrogen or special cases, e.g. multiple or low purity N ₂
2205/80	• using membrane, i.e. including a permeation step	2215/44	• • Ultra high purity nitrogen, i.e. generally less than 1 ppb impurities
2205/82	• using a reactor with combustion or catalytic reaction	2215/50	• Oxygen or special cases, e.g. isotope-mixtures or low purity O ₂
2205/84	• using filter	2215/52	• • Oxygen production with multiple purity O ₂
2205/86	• using electrical phenomena, e.g. Corona discharge, electrolysis or magnetic field	2215/54	• • Oxygen production with multiple pressure O ₂
2205/90	• Mixing of components	2215/56	• • Ultra high purity oxygen, i.e. generally more than 99,9% O ₂
2210/00	Processes characterised by the type or other details of the feed stream (not used)	2215/58	• Argon
2210/02	• Multiple feed streams, e.g. originating from different sources	2215/60	• Methane
2210/04	• Mixing or blending of fluids with the feed stream	2215/62	• Ethane or ethylene
2210/06	• Splitting of the feed stream, e.g. for treating or cooling in different ways	2215/64	• Propane or propylene
2210/12	• Refinery or petrochemical off-gas	2215/66	• Butane or mixed butanes
2210/14	• Coke-ovens gas	2215/80	• Carbon dioxide
2210/18	• H ₂ /CO mixtures, i.e. synthesis gas; Water gas, shifted synthesis gas or purge gas from HYCO synthesis	2220/00	Processes or apparatus involving steps for the removal of impurities (not used)
2210/20	• H ₂ /N ₂ mixture, i.e. synthesis gas for or purge gas from ammonia synthesis	2220/02	• Separating impurities in general from the feed stream
2210/40	• Air or oxygen enriched air, i.e. generally less than 30mol% of O ₂	2220/04	• Separating impurities in general from the product stream
2210/42	• Nitrogen	2220/40	• Separating high boiling, i.e. less volatile components from air, e.g. CO ₂ , hydrocarbons
2210/50	• Oxygen	2220/42	• Separating low boiling, i.e. more volatile components from nitrogen, e.g. He, H ₂ , Ne
2210/58	• Argon	2220/44	• Separating high boiling, i.e. less volatile components from nitrogen, e.g. CO, Ar, O ₂ , hydrocarbons
2210/60	• Natural gas or synthetic natural gas [SNG]	2220/50	• Separating low boiling, i.e. more volatile components from oxygen, e.g. N ₂ , Ar
2210/62	• Liquefied natural gas [LNG]; Natural gas liquids [NGL]; Liquefied petroleum gas [LPG]	2220/52	• Separating high boiling, i.e. less volatile components from oxygen, e.g. Kr, Xe, Hydrocarbons, Nitrous oxides, O ₃
2210/66	• Landfill or fermentation off-gas, e.g. "Bio-gas"	2220/60	• Separating impurities from natural gas, e.g. mercury, cyclic hydrocarbons
2210/70	• Flue or combustion exhaust gas	2220/62	• • Separating low boiling components, e.g. He, H ₂ , N ₂ , Air
		2220/64	• • Separating heavy hydrocarbons, e.g. NGL, LPG, C ₄ + hydrocarbons or heavy condensates in general
		2220/66	• • Separating acid gases, e.g. CO ₂ , SO ₂ , H ₂ S or RSH
		2220/68	• • Separating water or hydrates

- 2220/80 . Separating impurities from carbon dioxide, e.g. H₂O or water-soluble contaminants
- 2220/82 . . Separating low boiling, i.e. more volatile components, e.g. He, H₂, CO, Air gases, CH₄
- 2220/84 . . Separating high boiling, i.e. less volatile components, e.g. NO_x, SO_x, H₂S
- 2220/90 . Separating isotopes of a component, e.g. H₂, O₂
- 2230/00 Processes or apparatus involving steps for increasing the pressure of gaseous process streams (not used)**
- 2230/02 . Compressor intake arrangement, e.g. filtering or cooling
- 2230/04 . Compressor cooling arrangement, e.g. inter- or after-stage cooling or condensate removal
- 2230/06 . Adiabatic compressor, i.e. without interstage cooling
- 2230/08 . Cold compressor, i.e. suction of the gas at cryogenic temperature and generally without afterstage-cooler
- 2230/20 . Integrated compressor and process expander; Gear box arrangement; Multiple compressors on a common shaft
- 2230/22 . Compressor driver arrangement, e.g. power supply by motor, gas or steam turbine
- 2230/24 . Multiple compressors or compressor stages in parallel
- 2230/30 . Compression of the feed stream
- 2230/32 . Compression of the product stream
- 2230/40 . the fluid being air
- 2230/42 . the fluid being nitrogen
- 2230/50 . the fluid being oxygen
- 2230/52 . the fluid being oxygen enriched compared to air, e.g. "crude oxygen"
- 2230/58 . the fluid being argon or crude argon
- 2230/60 . the fluid being hydrocarbons or a mixture of hydrocarbons
- 2230/80 . the fluid being carbon dioxide
- 2235/00 Processes or apparatus involving steps for increasing the pressure or for conveying of liquid process streams (not used)**
- 2235/02 . using a pump in general or hydrostatic pressure increase
- 2235/04 . using a pressure accumulator
- 2235/06 . Lifting of liquids by gas lift, e.g. "Mammutpumpe"
- 2235/42 . the fluid being nitrogen
- 2235/50 . the fluid being oxygen
- 2235/52 . the fluid being oxygen enriched compared to air ("crude oxygen")
- 2235/58 . the fluid being argon or crude argon
- 2235/60 . the fluid being (a mixture of) hydrocarbons
- 2235/80 . the fluid being carbon dioxide
- 2240/00 Processes or apparatus involving steps for expanding of process streams (not used)**
- 2240/02 . Expansion of a process fluid in a work-extracting turbine (i.e. isentropic expansion), e.g. of the feed stream
- 2240/04 . . Multiple expansion turbines in parallel
- 2240/10 . . the fluid being air
- 2240/12 . . the fluid being nitrogen
- 2240/20 . . the fluid being oxygen
- 2240/22 . . the fluid being oxygen enriched compared to air, e.g. "crude oxygen"
- 2240/28 . . the fluid being argon or crude argon
- 2240/30 . Dynamic liquid or hydraulic expansion with extraction of work, e.g. single phase or two-phase turbine
- 2240/40 . Expansion without extracting work, i.e. isenthalpic throttling, e.g. JT valve, regulating valve or venturi, or isentropic nozzle, e.g. Laval
- 2240/42 . . the fluid being air
- 2240/44 . . the fluid being nitrogen
- 2240/46 . . the fluid being oxygen
- 2240/48 . . the fluid being oxygen enriched compared to air, e.g. "crude oxygen"
- 2240/60 . Expansion by ejector or injector, e.g. "Gasstrahlpumpe", "venturi mixing", "jet pumps"
- 2240/70 . Steam turbine, e.g. used in a Rankine cycle
- 2240/80 . Hot exhaust gas turbine combustion engine
- 2240/82 . . with waste heat recovery, e.g. in a combined cycle, i.e. for generating steam used in a Rankine cycle
- 2240/90 . Hot gas waste turbine of an indirect heated gas for power generation
- 2245/00 Processes or apparatus involving steps for recycling of process streams (not used)**
- 2245/02 . Recycle of a stream in general, e.g. a by-pass stream
- 2245/40 . the recycled stream being air
- 2245/42 . the recycled stream being nitrogen
- 2245/50 . the recycled stream being oxygen
- 2245/58 . the recycled stream being argon or crude argon
- 2245/90 . the recycled stream being boil-off gas from storage
- 2250/00 Details related to the use of reboiler-condensers (not used)**
- 2250/02 . Bath type boiler-condenser using thermo-siphon effect, e.g. with natural or forced circulation or pool boiling, i.e. core-in-kettle heat exchanger
- 2250/04 . Down-flowing type boiler-condenser, i.e. with evaporation of a falling liquid film
- 2250/10 . Boiler-condenser with superposed stages
- 2250/20 . Boiler-condenser with multiple exchanger cores in parallel or with multiple re-boiling or condensing streams
- 2250/30 . External or auxiliary boiler-condenser in general, e.g. without a specified fluid or one fluid is not a primary air component or an intermediate fluid
- 2250/40 . . One fluid being air
- 2250/42 . . One fluid being nitrogen
- 2250/50 . . One fluid being oxygen
- 2250/52 . . One fluid being oxygen enriched compared to air, e.g. "crude oxygen"
- 2250/58 . . One fluid being argon or crude argon
- 2260/00 Coupling of processes or apparatus to other units; Integrated schemes (not used)**
- 2260/02 . Integration in an installation for exchanging heat, e.g. for waste heat recovery
- 2260/10 . Integration in a gas transmission system at a pressure reduction, e.g. "let down" station
- 2260/20 . Integration in an installation for liquefying or solidifying a fluid stream
- 2260/30 . Integration in an installation using renewable energy

- 2260/42 . Integration in an installation using nitrogen, e.g. as utility gas, for inerting or purging purposes in IGCC, POX, GTL, PSA, float glass forming, incineration processes, for heat recovery or for enhanced oil recovery
- 2260/44 . . using nitrogen for cooling purposes
- 2260/50 . Integration in an installation using oxygen, e.g. in the burner of a glass facility, waste incineration or oxygen based process [OBP] in general
- 2260/58 . Integration in an installation using argon
- 2260/60 . Integration in an installation using hydrocarbons, e.g. for fuel purposes
- 2260/80 . Integration in an installation using carbon dioxide, e.g. for EOR, sequestration, refrigeration etc.
- 2270/00 Refrigeration techniques used (not used)**
- 2270/02 . Internal refrigeration with liquid vaporising loop
- 2270/04 . Internal refrigeration with work-producing gas expansion loop
- 2270/06 . . with multiple gas expansion loops
- 2270/08 . Internal refrigeration by flash gas recovery loop
- 2270/12 . External refrigeration with liquid vaporising loop
- 2270/14 . External refrigeration with work-producing gas expansion loop
- 2270/16 . . with multiple gas expansion loops of the same refrigerant
- 2270/18 . External refrigeration with incorporated cascade loop
- 2270/20 . Quasi-closed internal or closed external hydrogen refrigeration cycle
- 2270/24 . Quasi-closed internal or closed external carbon monoxide refrigeration cycle
- 2270/30 . Quasi-closed internal or closed external helium refrigeration cycle
- 2270/40 . Quasi-closed internal or closed external air refrigeration cycle
- 2270/42 . Quasi-closed internal or closed external nitrogen refrigeration cycle
- 2270/50 . Quasi-closed internal or closed external oxygen refrigeration cycle
- 2270/58 . Quasi-closed internal or closed external argon refrigeration cycle
- 2270/60 . Closed external refrigeration cycle with single component refrigerant [SCR], e.g. C1-, C2- or C3-hydrocarbons
- 2270/66 . Closed external refrigeration cycle with multi component refrigerant [MCR], e.g. mixture of hydrocarbons
- 2270/80 . Quasi-closed internal or closed external carbon dioxide refrigeration cycle
- 2270/88 . Quasi-closed internal refrigeration or heat pump cycle, if not otherwise provided
- 2270/90 . External refrigeration, e.g. conventional closed-loop mechanical refrigeration unit using Freon or NH₃, unspecified external refrigeration
- 2270/902 . . Details about the refrigeration cycle used, e.g. composition of refrigerant, arrangement of compressors or cascade, make up sources, use of reflux exchangers etc.
- 2270/904 . . by liquid or gaseous cryogen in an open loop
- 2270/906 . . by heat driven absorption chillers
- 2270/908 . . by regenerative chillers, i.e. oscillating or dynamic systems, e.g. Stirling refrigerator, thermoelectric ("Peltier") or magnetic refrigeration
- 2270/91 . . . using pulse tube refrigeration
- 2270/912 . . Liquefaction cycle of a low-boiling (feed) gas in a cryocooler, i.e. in a closed-loop refrigerator
- 2280/00 Control of the process or apparatus (not used)**
- 2280/02 . Control in general, load changes, different modes ("runs"), measurements
- 2280/10 . Control for or during start-up and cooling down of the installation
- 2280/20 . Control for stopping, deriming or defrosting after an emergency shut-down of the installation or for back up system
- 2280/30 . Control of a discontinuous or intermittent ("batch") process
- 2280/40 . Control of freezing of components
- 2280/50 . Advanced process control, e.g. adaptive or multivariable control
- 2290/00 Other details not covered by groups**
[F25J 2200/00](#) - [F25J 2280/00](#) (not used)
- 2290/02 . Comparison of processes or apparatuses
- 2290/10 . Mathematical formulae, modeling, plot or curves; Design methods
- 2290/12 . Particular process parameters like pressure, temperature, ratios
- 2290/20 . Particular dimensions; Small scale or micro devices
- 2290/30 . Details about heat insulation or cold insulation
- 2290/32 . Details on header or distribution passages of heat exchangers, e.g. of reboiler-condenser or plate heat exchangers
- 2290/34 . Details about subcooling of liquids
- 2290/40 . Vertical layout or arrangement of cold equipments within in the cold box, e.g. columns, condensers, heat exchangers etc.
- 2290/42 . Modularity, pre-fabrication of modules, assembling and erection, horizontal layout, i.e. plot plan, and vertical arrangement of parts of the cryogenic unit, e.g. of the cold box
- 2290/44 . Particular materials used, e.g. copper, steel or alloys thereof or surface treatments used, e.g. enhanced surface
- 2290/50 . Arrangement of multiple equipments fulfilling the same process step in parallel
- 2290/60 . Details about pipelines, i.e. network, for feed or product distribution
- 2290/62 . Details of storing a fluid in a tank
- 2290/70 . Processing device is mobile or transportable, e.g. by hand, car, ship, rocket engine etc.
- 2290/72 . Processing device is used off-shore, e.g. on a platform or floating on a ship or barge
- 2290/80 . Retrofitting, revamping or debottlenecking of existing plant
- 2290/90 . Details about safety operation of the installation